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Published in:

Tanzania Journal of Engineering and Technology

2019

Document Version:

Publisher's PDF, also known as Version of record

[Link to publication](#)

Citation for published version (APA):

Mdkude, I., Mbwette, T., Gabrielsson, S., & Kimwaga, R. (2019). Material Flow Analysis as a Decision Supporting tool for Faecal Sludge Resource Recovery: Mathematical formulation and quantification. *Tanzania Journal of Engineering and Technology*, 38(1), 97-115. Article Vol 38 (1).

Total number of authors:

4

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Full Length Research Paper

Material Flow Analysis as a Decision Supporting tool for Faecal Sludge Resource Recovery: Mathematical formulation and quantification

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ABSTRACT

In this work, a conceptual framework for faecal sludge (FS) management and resource recovery in Dar es Salaam city was developed. Material Flow Analysis (MFA) approach was used to assess and quantify the current materials and nutrients to support on decisions for nutrient recovery and minimize environmental pollution in three unplanned settlements of Manzese, Keko and Kipawa in Dar es Salaam city. Nitrogen and Phosphorus were chosen as indicators for the evaluation of the process. The results showed that about 75% of the Dar es Salaam city population relies on pit latrines and 15% connected to septic tanks, translating to a large amount of faecal sludge being contained onsite. The situational analysis study on faecal sludge management (FSM) showed that the collection, treatment and proper disposal of FS are the major challenges that pose risks to public health. Currently, 57% of faecal sludge generated in Dar es Salaam is disposed to the environment inappropriately. Onsite Sanitation Systems in all study areas are the main polluters, discharging large quantity of nutrients to the environment. About 37.7% of faecal sludge is with large amount of nutrients emptied from onsite sanitation systems discharged to the environment and through seepage to the groundwater.

Keywords: Faecal sludge; Material flow analysis; Resource recovery; unplanned settlements.

INTRODUCTION

Faecal sludge (FS) is an organic material that can be reused as organic fertilizer, source of energy or source of protein for animal feeds (Diener *et al.*, 2014), which can contribute to solving soil degradation, food insecurity, environmental pollution and lack of energy access challenges (Munamati *et al.*, 2016). Nitrogen and Phosphorus are nutrients in faecal sludge, which are estimated to be 8.2 g/L and 1.1 g/L, respectively of dry faecal sludge (Andriani *et al.*, 2015). About 50-90% of

organic matter in FS possesses the recovery opportunities.

Chemical fertilizer is one among must-have commodity for most African farmers in increasing soil fertility and crop production, but it is expensive which calls for a substitute cheaper material. On the other hand, access to urban domestic energy sources is a challenge resulting to dependency on solid fuels as a source of energy for cooking across urban areas in Africa followed by gas and liquid fuels (Drechsel *et al.*, 2004). The need for

resources recovery from faecal sludge is an opportunity that can integrate new ideas and technology with existing sanitation collection and treatment systems. Through thermal decomposition, FS sludge material can successfully be processed for energy recovery because of its rich carbon content (Kwapinski *et al.*, 2010) to substitute with the use of firewood, charcoal or other solid fuels (Gold *et al.*, 2018; Liu *et al.*, 2014) and contributing in saving money, decrease local deforestation rates and provide income generating opportunity (Nyer, 2012).

To assess resource consumption and environmental impacts of resources from sanitation systems, Material Flow Analysis (MFA) method that uses quantitative procedures to systematically assess matter and substances within a system can be used (Do-thu *et al.*, 2011; Strauss and Montangero, 2002). This tool has been widely applied in the field of environmental sanitation in urban areas and in industrial processes of developing countries since the 1990s (Montangero and Belevi, 2007; Do-thu *et al.*, 2011). MFA approach assists the decision making by estimating the total quantities of reuse products to be produced.

About 90% of Dar es Salaam population relies on onsite sanitation systems while only 43% of generated faecal sludge is collected and safely treated in Waste Stabilization Ponds (WSPs) (Brandes *et al.*, 2015). At the endpoints of WSP, recovery of treated liquid effluents is informally utilized in urban agricultural activities, growing leafy vegetables like Amaranth, pumpkin leaves and okra along water sources including Msimbazi, Mzinga, Kizinga and Ng'ombe rivers, in-plots and on backyard gardens (Dongus *et al.*, 2009; Leonard *et al.*, 2012). However, the quality of water is still questionable because several researchers have reported

the presence of pathogenic organisms in these vegetables, which might pose potential human health risks (Kayombo and Mayo, 2018; Malale and Munishi, 2018).

The large amount of piled up treated semi-solid part of faecal sludge from WSPs is another management challenge that municipalities are facing (Gold *et al.*, 2014). This can be taken as recovery opportunity to produce soil conditioning material or solid fuel for cooking instead of disposing it to the environment (Atwijukye *et al.*, 2018; Niwagaba *et al.*, 2009; Niwagaba *et al.*, 2014). The objective of this study was to quantify materials flow to the households and nutrients (nitrogen and phosphorus) through the sanitation service chain in order to contribute to the decision making on the process for pollution mitigating measures. The emphasis in this study was the concept of resource reuse efficiency in sanitation in unplanned settlements of Dar es Salaam city.

MATERIALS AND METHODS

Description of Study Areas

The targeted study areas were three unplanned settlements in Dar es Salaam city, namely Manzese, Keko and Kipawa, located in Ubungo, Temeke and Ilala Municipalities, respectively (Figure 1). The study area covers an area of 19 km² with an estimated total population of 224,140 (NBS, 2017). Three wards represent typical middle to low-income communities living in urban unplanned settlements of Dar es Salaam. These areas are densely populated with both residential and commercial buildings. A large portion of grey water is directed to either onsite sanitation facilities or disposed of to the environment through open channels or pipes (Kasala, 2016).

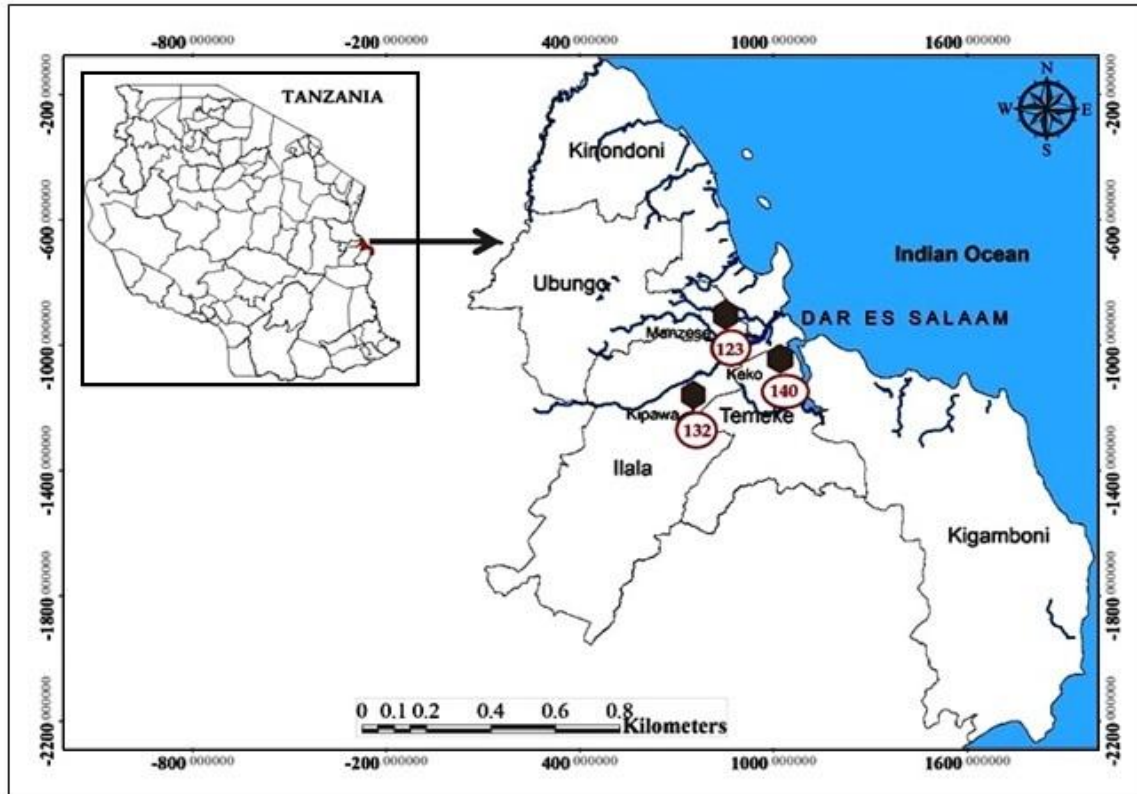


Figure 1: Location of study areas and sampling points for the household survey.

Data Collection and Analysis

The mixed-method of data collection was deployed for both qualitative and quantitative data collected between September 2017 and November 2018. Key informants’ interviews with sanitation stakeholders were conducted to assess the City-wise practices on faecal sludge management and plans along the sanitation service chain. The questionnaire survey was conducted by using mobile phone application known as *Epicollect5*. The sample size for the questionnaire survey was obtained using the equation (1).

$$n = \frac{N}{1+N(\alpha)^2} \dots\dots\dots (1)$$

Where n = sample size, N = total number of houses/population/units to be studied; 70% of total population (Brandes *et al*, 2015) and α = the margin of error or desired level of precision, at confidence level of 95% is $\pm 5\%$ (de Langen, 2007). A

total number of 400 respondents (n) was obtained, which was proportionally distributed in three study areas according to the present population of the area. The households’ samples were randomly selected.

The administered questionnaires contained five parts which seek primary information from study population including; (i) Socio-economic characteristics, (ii) Sanitation and water use, (iii) Community engagement to sanitation and FSM activities (iv) Community health and (v) Sustainable sanitation and resource recovery. Focus group discussions were conducted to gather information on the insights from the community about knowledge, challenges, and opportunities available on resource recovery plans and preferences on faecal-based products. Secondary information on nitrogen and phosphorus concentrations estimations and

calculations in different materials (food, water and faecal sludge) used from published documents as well as institutional and national reports available online and in the offices were also identified and used. Assumptions made and relevant information adopted was stated in respective areas when they were used.

After collection, data were extracted and saved as Microsoft Excel 2010 spread sheet file. The file was coded and manually double-checked to eliminate the risk of any mistakes. The Statistical Package for Social Science (SPSS 21) was used to calculate the frequencies and relative frequency of responses.

Material Flow Analysis (MFA) System

MFA system under investigation defined the spatial boundary of three selected administrative wards and one year as a temporal boundary. The mass flows of materials such as water and food and substances such as nitrogen and phosphorus were calculated through a defined system. All calculations for

quantification were performed by Microsoft Excel program Version 2010 following different mathematical formulae while mass balances and pictorial representations were performed by Software for Substance Flow Analysis (STAN) version 2.1 (Cencic and Rechberger, 2008). Processes under MFA are represented by boxes while flows are represented by arrows. No stock amount from the previous year of materials and substances were considered in the calculations. To quantify stocks and flows, each particular material was identified as a whole or with ratios allocated to different processes (Allesch and Brunner, 2015).

The scenario represents current situation system consists of 5 processes with 13 flows (Figure 2). However, surface water, ground water and atmosphere processes were not considered because they are beyond the system boundaries and scope of this study. The impact of environmental sanitation systems on the nitrogen and phosphorus load was analyzed from the rest of the processes.

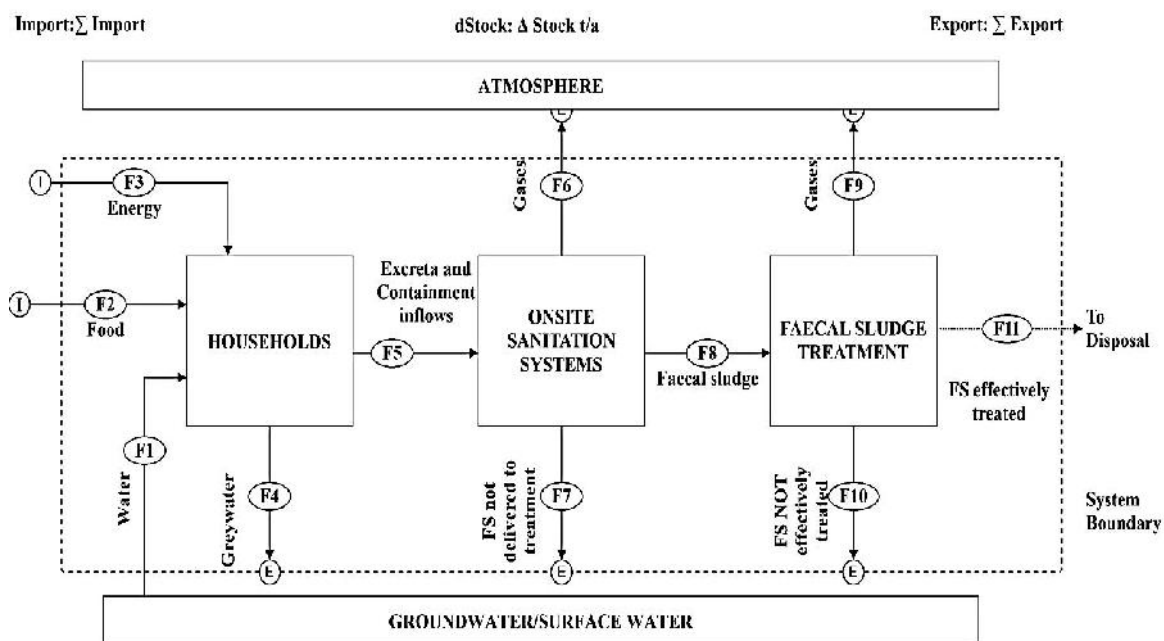


Figure 2: Material flow analyses for current situation scenario

Mathematical Formulation

Material Flow Analysis follows the law of conservation of mass. All inputs, stocks and outputs data of a process were obtained from different sources and calculated using mathematical formulae under each process. The uncertainty analysis was performed to propagate uncertainties for MFA inputs so as to determine distribution of outputs depending on the source of data to be used. When variable obtained contains arithmetic mean value (\bar{X}) and standard deviation (SD) calculated from data set available, the uncertainty (U_r) calculated using Gauss error traditional approach by dividing (SD) with (\bar{X}) times 100%. If no uncertainty defined for a particular parameter and only lower and upper bounds available, a general uncertainty of 10% was assumed as suggested by Meininger (2010). All data calculated included the uncertainty value in form of $\bar{X} \pm U_r$.

Households

Potable water (F1), food supply (F2) and energy sources for kitchen use needed in the house (F3) were the inputs to households, while greywater (F4) and excreta with containment inflows (F5) were the outputs. The average water consumption per capita per day was obtained from the household questionnaire survey as volume (L/d) converted to mass unit considering 1000 kg/m³ as a density of water (Cencic and Rechberger, 2008).

Food amount was calculated by summing up annual per capita food items supplied under the current Tanzania Food Balance sheet estimated by the Food and Agriculture Organization (FAO, 2013). The energy sources considered at household level was wood charcoal based on dominant energy source requirement for kitchen purposes obtained from a questionnaire survey. The value of wood charcoal was extrapolated from the amount

reported by Msuya *et al.* (2011) using the current population and calorific values the amount of energy source, which was obtained from equation (2) in accordance with Meininger (2010).

$$C_c = \frac{E_c}{C_{HV}} \dots\dots\dots (2)$$

where E_c = Current energy demand from wood charcoal (kWh/cap/yr), C_c = Current consumption of charcoal (t/cap/yr) and C_{HV} = heating value of charcoal (kWh/kg).

Greywater generation from dishwashing and laundry activities was estimated on assumption that 65% to 75% of domestic water consumption was converted to greywater (Chaggu, 2004; Diener *et al.*, 2014; Do-thu *et al.*, 2011; Katukiza, 2013). Adopting 75% of water consumption, the total greywater generated in this study was calculated. The amount of excreta production was calculated from equation (3) using secondary data of similar locality of developing countries (Marwa, 2017; Schoebitz *et al.*, 2014).

$$E_p = U_p + F_p \dots\dots\dots (3)$$

where E_p = excreta produced (kg/cap/d); U_p = urine produced (kg/cap/d) and F_p = faeces produced (kg/cap/d).

Containment inflow is the amount of black water that goes out of the toilet together with excreta to sanitation systems. This includes water used for anal cleansing and bathing, which is discharged to onsite sanitation systems. Nitrogen and phosphorus are the major nutrients proposed for assessment. Nitrogen enters household mainly through food while phosphorus enters through food and other sources like detergents used for cleaning and laundry activities. The general nitrogen and phosphorus mass balance equations in the process are expressed by equations (4) and (5), which considers all input and output flows.

$$A_{NF1} + A_{NF2} + A_{NF3} = A_{NF4} + A_{NF5} ;$$

..... (4)

$$A_{PF1} + A_{PF2} + A_{PF3} = A_{PF4} + A_{PF5}$$

..... (5)

where A_N and A_P are the amounts of Nitrogen and Phosphorus flowing through flows (F1), (F2), (F3), (F4) and (F5), respectively.

Onsite sanitation systems

Excreta and containment inflows (F5) are the only inputs to onsite sanitation systems (OSSs). Rainwater inflows and solid waste inputs were neglected in calculations for this case. The outputs from the onsite

sanitation system process are gases emitted (F6), total faecal sludge emptied and delivered to treatment plants (F8) and fraction of faecal sludge which was not delivered to treatment plants (F10).

The total faecal sludge generated is a function of excreta produced and containment inflows, which is the amount of blackwater disposed to the onsite sanitation systems (Marwa, 2017; Schoebitz *et al.*, 2014). A summarised findings from the survey on fraction distribution of generated faecal sludge in study areas is presented in Table 1.

Table 1: Fraction distribution of generated faecal sludge

Study areas		Keko	Kipawa	Manzese	Reference
Population		79,453	74,180	70,507	NBS (2017)
Fraction of pit latrines available (%)		27.1%	35.9%	61.8%	This study
Fraction of septic tanks available (%)		72.1%	63.4%	38.2%	This study
FS generated (kg/cap/d)		9.65 ± 1.34	11.38 ± 1.85	8.65 ± 1.59	This study
	% of generated FS	43%	39%	76%	This study
FS emptied (kg/cap/d)		4.15 ± 0.58	4.44 ± 0.72	6.57 ± 1.21	This study
FS emptied-delivered to treatment points (kg/cap/d)	27% of FS Emptied	1.12 ± 0.16	1.19 ± 0.19	1.77 ± 0.33	Brandes <i>et al.</i> (2015)
FS emptied- NOT delivered to treatment points (kg/cap/d)	73% of FS Emptied	3.03 ± 0.42	3.24 ± 0.53	4.79 ± 0.88	Brandes <i>et al.</i> (2015); Jenkins <i>et al.</i> (2015).
FS not emptied- not contained -seepage & illegal disposal (kg/cap/d)	11.2% of FS generated	1.08±0.15	1.27±0.21	0.97±0.18	Brandes <i>et al.</i> (2015)
FS not Emptied- Stock (kg/cap/d)	37.2% of FS generated	3.57±0.50	4.21±0.68	3.20±0.59	Brandes <i>et al.</i> (2015); Jenkins <i>et al.</i> (2015).

Methane (CH₄) gas can be emitted from onsite anaerobic sanitation systems when methanogens become active at a temperature above 15°C (Orner and Mihelcic, 2018). The estimation of methane emission from latrines (traditional and VIPs) is a function of the daily mass of biochemical oxygen demand (BOD) in the influent, organic matter removal efficiency and other conversion factors.

IPCC Guidelines for National Greenhouse Gas presents simplified general equations to estimate CH₄ emissions from domestic wastewater (IPCC, 2006) in accordance with equation (6).

$$CH_4 \text{ emission} = (BOD_T \times B_o \times MCF) - R$$

..... (6)

where CH₄ emissions = CH₄ emissions in inventory year in kg CH₄/yr, BOD_T = Total organics in wastewater in inventory year in kg BOD/yr, R = amount of CH₄ recovered/recycled in inventory year in kg CH₄/yr. No recycling was performed, hence R was assumed to be zero, Bo = maximum CH₄ producing capacity in kg CH₄/kg BOD; given 0.6 kg CH₄/kg BOD as default, MCF = methane correction factor (fraction), which was assumed to be 0.5 for septic tanks (half of BOD settles in an anaerobic tank), and 0.7 for pit latrine (wet climate/flush water use, higher groundwater table).

To balance Nitrogen and Phosphorus amounts in onsite sanitation systems process (OSSs), equations (7) and (8) were used to consider all input and output flow.

$$A_{NF5} = A_{NF6} + A_{NF7} + A_{NF8} \dots \dots (7)$$

$$A_{PF5} = A_{PF6} + A_{PF7} + A_{PF8} \dots \dots (8)$$

where the A_N and A_P are the amount of Nitrogen and Phosphorus flowing through flows (F5), (F6), (F7) and (F8), respectively.

Different conditions occur inside specific onsite sanitation systems. In the septic tank, settling and partial decomposition of organic matter occurs while the accumulation of solids and infiltration of liquid occurs in pit latrines (Montangero *et al.*, 2007). Transfer coefficients for each nutrient (*kN*) and (*kP*) should be considered depending on physical and

biochemical processes that occur in different sanitation systems. Transfer coefficients for nutrients from both septic tanks and pit latrines are partitioned into leachate and sludge. Depending on the local conditions of specific areas, different ranges exist as reported by previous studies (Montangero, 2006; Montangero and Belevi, 2007; Montangero and Belevi, 2008).

The adopted coefficients to use for Nitrogen, *kN* and Phosphorus, *kP* selected as 0.09 and 0.18 for septic tanks respectively. The *kN* = 0.18 and *kP* = 0.29 were also selected for pit latrine. Other conditions considered were fraction of septic tanks (*n_{ST}*) and pit latrines (*n_{PL}*) available in the area (Table 1) and faecal sludge emptying frequency factor for each facility; septic tanks (*F_{fr-ST}*) and pit latrines (*F_{fr-PL}*). An average emptying frequency of once in 2 years was adopted for septic tanks (*F_{fr-ST}* = 2) (Montangero, 2009). Due to the high groundwater table in the study areas, emptying frequency of pit latrines was reported to be three times per year (*F_{fr-PL}* = 0.33).

The mass of nutrients flowing in flow (F7) and (F8) were estimated using equations (9) and (10), respectively. The output flows from OSS process include emptied and delivered to treatment plants (F8) and that not delivered to the treatment (F7). All fractions of faecal sludge in study areas are as presented in Table 1.

$$A_{NF7} \text{ and } A_{NF8} = (n_{ST}) \cdot A_{N(fS)}^{ST} + (n_{PL}) \cdot A_{N(fS)}^{PL} \dots \dots \dots (9)$$

$$A_{PF7} \text{ and } A_{PF8} = (n_{ST}) \cdot A_{P(fS)}^{ST} + (n_{PL}) \cdot A_{P(fS)}^{PL} \dots \dots \dots (10)$$

where the amounts of nitrogen and phosphorus in (F7) and (F8) consider both pit latrines and septic tanks fractions available.

Faecal sludge treatment

The input to faecal sludge treatment plants is a reported fraction of faecal sludge which was emptied and reached wastewater treatment plants for treatment

(F8). The outputs include gases generated and emitted during treatment processes (F9), treated effluent to water bodies (F11) and part of effluent which was not effectively treated, but disposed to water bodies (F10). Currently, faecal sludge collected in Dar es Salaam is transported to Waste Stabilization Ponds for secondary treatment before the effluent is discharged into the rivers (Brandes *et al.*, 2015). Two WSPs which are designated for FS treatment are located at Vingunguti and Kurasini areas, with capacity of 2000 m³

and 135 m³/d of FS, respectively (Brandes *et al.*, 2015; EWURA, 2014).

Three primary greenhouse gases GHGs, i.e. methane (CH₄), carbon dioxide (CO₂) and nitrous oxide (N₂O) (Vijayan *et al.*, 2017) are likely to be produced from treatment systems or discharge pathways with anaerobic environments. Anaerobic ponds with depth 2-5 m are a critical factor in CH₄ production. Methane and carbon dioxide can be calculated using equations (11) and (12).

$$CO_2 = BOD \times Q_{ww} \times Eff_{OD} \times CF_{CO_2} \times [(1 - MCF_{ww} \times BG_{CH_4})(1 - \lambda)] \dots\dots\dots (11)$$

$$CH_4 = BOD \times Q_{ww} \times Eff_{OD} \times CF_{CH_4} \times [(MCF_{ww} \times BG_{CH_4})(1 - \lambda)] \dots\dots\dots (12)$$

where CO₂ and CH₄ are the air emissions (kg/yr), BOD is the daily mass of biochemical oxygen demand in the influent, which is reported to be 10 mg/l (10g/m³) for Vingunguti WSP (Mwakaboko *et al.* 2014), Q_{ww} is wastewater influent flow rate (m³/d), which is the capacity of Vingunguti WSP = 2000 m³/d (Brandes *et al.*, 2015; EWURA 2014). Q_{ww} calculated from three study areas inclusively is 0.0026 m³/cap/d, which was converted from mass of FS (F8), Eff_{OD} is the biochemical oxygen demand removal efficiency (default assumed 80%), CF_{CO₂} is the conversion factor for maximum CO₂ generation per unit of BOD (1.375 g CO₂ per g BOD), CF_{CH₄} is the conversion factor for maximum CH₄ generation per unit of BOD (0.5 g CH₄ g BOD⁻¹). BG_{CH₄} is the fraction of carbon present as CH₄ in generated biogas (default is 65%),

MCF_{ww} is the methane correction factor for a wastewater treatment unit usually 0.8 for anaerobic conditions and is the biomass yield (g C converted to biomass per g C consumed), also specific to each treatment unit, which is suggested to be 0.1 for anaerobic conditions.

Nitrous oxide (N₂O) can be emitted directly from treatment plants or indirectly from wastewater after disposal of the effluent to the receiving body (IPCC, 2006). Amount of gases emitted for this case considered indirect emission of effluent to receiving bodies and are function of nitrogen content in the wastewater effluent, population and average annual per capita protein generation (kg/person/yr). Using equations (13) and (14), the emission of nitrous oxide can be estimated.

$$N_2O_{WWTP} = N_{EFFLUENT} \times EF_{N_2O} \times \frac{44}{28} \dots\dots\dots (13)$$

$$N_{EFFLUENT} = (Ca \times Protein \times F_{NPR} \times F_{NON_CON} \times F_{IND_COM}) - N_{SLUDGE} \dots\dots\dots (14)$$

where N₂O_{WWTP} = N₂O emissions in inventory year (kg N₂O/yr), N_{EFFLUENT} = total annual amount of nitrogen in the wastewater effluent (kg N/yr), EF_{N₂O} = Emission factor (gN emitted as N₂O per g

TKN in influent). Based on limited data and assumptions on nitrification and denitrification in rivers, the default IPCC emission factor for N₂O emissions from domestic wastewater nitrogen effluent is

0.005 (0.0005 - 0.25) kg N₂O-N/kg N, The factor 44/28 is the conversion of kg N₂O-N into kg N₂O, **N_{EFFLUENT}** = total annual amount of nitrogen in the wastewater effluent (kg N/yr), Protein = annual per capita protein consumption (kg/cap/yr). Given 57.8 g/cap/d (FAO, 2013) which is 21.1 kg/cap/yr, **F_{NPR}**= fraction of nitrogen in protein, default = 0.16 kg N/kg protein, **F_{NON_CON}** = factor for non-consumed protein added to the wastewater, 1.4 for countries with garbage disposals, **F_{IND_COM}** = factor for the industrial and commercial co-discharged protein into the sewer system. A factor to allow for co-discharge of industrial nitrogen into sewers, 1.25 and **N_{SLUDGE}** = nitrogen removed with sludge (default = zero) in kg N/yr.

Dar es Salaam Water Supply and Sanitation Authority (DAWASA) monitors and reports only Biological Oxygen Demand (BOD) parameter from WSPs effluent of Dar es Salaam (EWURA, 2017), hence no information on nutrients monitoring was available. However, a primary main function of maturation ponds is to remove pathogens from the wastewater (Mara 1984), but since they are oxygenated throughout the day, they contribute to nutrient removal and a small degree of BOD removal.

The general balance equations for nitrogen and phosphorus in the treatment plant process is expressed by equations (15) and (16), respectively. Nitrogen and phosphorus flowing through flows (F8), (F9), (F10) and (F11), respectively.

$$A_{NF8} = A_{NF9} + A_{NF10} + A_{NF11} \dots \dots \dots (15)$$

$$A_{PF8} = A_{PF9} + A_{PF10} + A_{PF11} \dots \dots \dots (16)$$

where (**A_N**) and (**A_P**) are amount of total nitrogen and phosphorus removal from WSPs varies depending on the status and functionality of the WSPs (Tarimo, 2016). Phosphorus removal is associated with algal biomass uptake, precipitation, and sedimentation (Mara *et al.*, 2010; von

Sperling, 2007). Nitrogen content in the effluent **A_{NF10}** and **A_{NF11}** are equal to **N_{EFFLUENT}**, which was calculated using equation (16). Brandes *et al.* (2015) reported that only 50% of faecal sludge delivered to treatment plants is effectively treated. The effluent from the treatment plant then is distributed equally by 0.50 treated while 0.50 is not effectively treated.

Phosphorus in the effluent from treatment plant (**A_{PF10}** ; **A_{PF11}**) is a function of the efficiency of WSP in remove of phosphorus (**P_{removal}** %). The initial amount entering the treatment plants (**A_{PF8}**) and the amount of FS to be treated (50% of **A_{PF8}**) as presented in equation (17).

$$A_{PF10} = 0.50 A_{PF8} \times (n_{P_removal} \%) \dots \dots \dots (17)$$

The overall nutrients removal efficiencies from anaerobic-facultative-maturation ponds given by von Sperling (2007) when assuming the WSPs work with the designing conditions, ranging from 50-65% for nitrogen and >50% for phosphorus. This study adopted the efficiency of (**n_{P_{removal}}**%) of 50% for phosphorus.

RESULTS AND DISCUSSION

Characteristics of Study Population

Socio-demographic characteristics

The average household occupancy from all the study areas was found to be 6 people. A single house consists of an average of 5 households with a total of 12 people. Respondents' age ranged from 18 to 82 years old with an average of 46.5 years old, 71.4% being women and 28.6% were men. More than a half of respondents have primary education and engaged on small businesses/entrepreneurship for economic generation activities. Level of education

and occupation for each study area are presented in Figures 4 and 5.

Water and sanitation situation

Potable water for domestic uses was obtained from both surface and groundwater sources and water availability varied with seasons and areas. The average water consumption for uses other than bathing was found to be 46.5 ± 27.9 L/cap/d and for bathing was determined to be 22.4 ± 9.1 L/cap/d.

Almost all houses (99.2%) depend on onsite sanitation systems including pit latrines and septic tanks. Manzese contains large percentage of pit latrine (61.8%) than septic tanks while in Keko and Kipawa more households use septic tanks than pit latrines. About 76% of sanitation facilities

in Manzese have already been desludged compared to Keko and Kipawa where less than 50% have been desludged.

Wastewater disposal location was found to be different in study areas. Table 2 shows percentage distribution of black water and greywater located to onsite sanitation system and used in calculating the nutrients flow in greywater.

Table 2: Wastewater disposal distribution to onsite sanitation system

	Black water only (%)	Black water and greywater (from bathing) (%)
Keko	17.9	82.0
Kipawa	20.6	79.3
Manzese	53.3	46.7

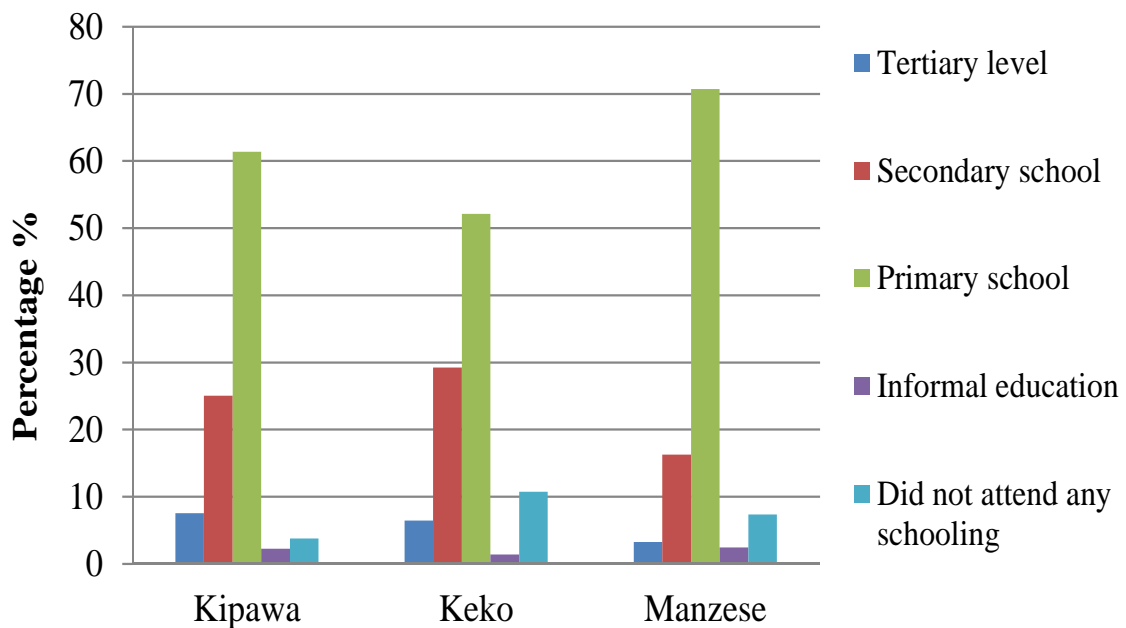


Figure 4: Percentage of respondents with education levels in each study area

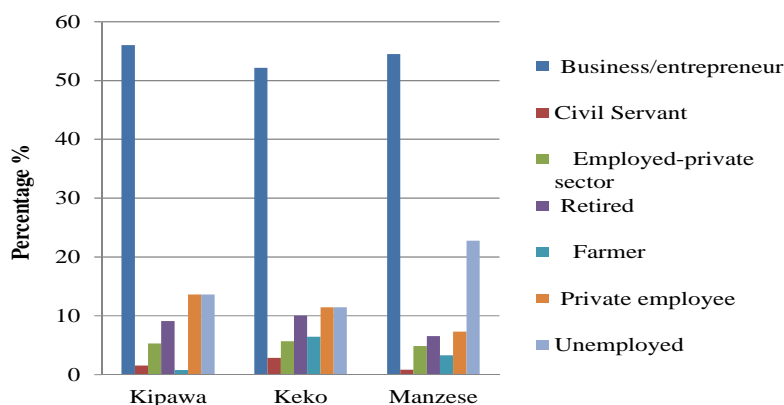


Figure 5: Percentage of respondents with occupations in each study area

Materials calculated

The mass balances for MFA was performed by STAN software using collected and calculated information. Materials flow through the system were calculated by considering combined information from three study areas as presented in Figure 6. All input, stock and output quantity of materials and nutrients estimated flowing to the system obey the law of conservation of mass. Nutrients flow were calculated and presented separately per study area for easier comparison. A summary of data inputs obtained through mathematical formulations and assumptions before mass balances are presented in Table 3.

The households are the main contributors of greywater discharge to the environment and water bodies. On average, each year a person consumes 16.9 kg of water from different sources and realises more than 30% of it as greywater to the environment. Yiougo *et al.* (2011) analyzed similar materials in Pouytenga town in Burkina Faso. It was found that about 7000 kg/cap/yr of water is consumed and 16%

of it is released as wastewater to surface water.

To reduce large amount of wastewater disposal to the environment (both greywater and faecal sludge), different options have been suggested. The separation and recycling of waste and wastewater at source can improve the situation (Meinzinger, 2010). As observed in this study, large amount of greywater from bathroom is also disposed to onsite sanitation system (Table 2), which is resulting into fast fill up of pits and therefore frequent requirement for desludging. It is suggested that separation of waste collected allows the reuse of separated greywater that comes from dishwashing and laundry activities for other activities that do not require good quality of potable water (Schaffner, 2007). However, transportation, energy and pre-treatment of materials before being reused might be needed, which have cost implications.

Poor management of faecal sludge from onsite sanitation system contributes to the

release of large amount of materials to groundwater and surface water. About 2.5 tons of faecal sludge contributed per person per year is released to the water sources without treatment. Most of toilet types found in study areas do not allow the use of vacuum tankers for desludging of pits and septic tanks contents because of

inaccessibility, lack of desludging points or the use of unlined pits, which encourages the practices of unhygienic desludging like manual emptying and flood out methods of pit contents to the nearby water sources. This might be the reason for large amount of faecal sludge not being accounted for treatment.

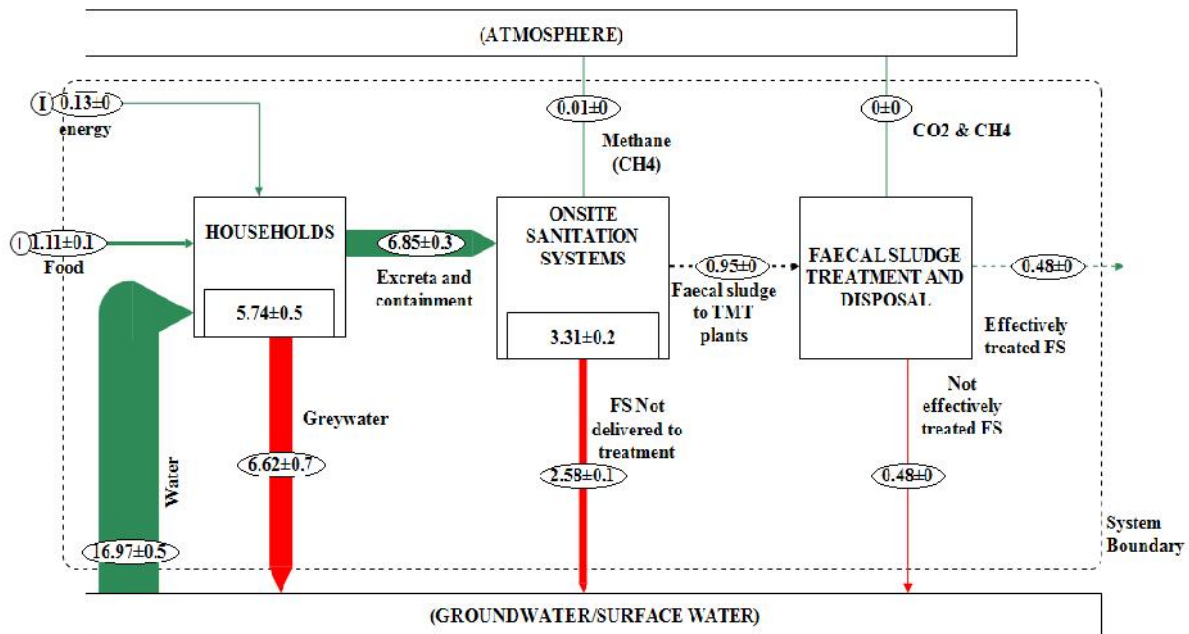


Figure 6: Mass of materials in current situation scenario of combine study areas (tons/cap/yr)

Figures 7 and 8 summarizes MFA of total nitrogen and phosphorus flows from households to treatment plants in three study areas. It was observed that in all study areas, the onsite sanitation systems (OSSs) were the main contributors and storage of materials with high amounts of nitrogen and phosphorus. This is due to the large amount of faecal sludge collected and stored within onsite sanitation system, which is about 48.3% of the generated faecal sludge (Figure 6). Through the sanitation service chain, large amount of nutrients is still emitted as a result of mismanagement of faecal sludge and wastewater. About 860 to 970 tons of nitrogen and 60 to 80 tons of phosphorus was discharged annually to the environment. The final treated FS effluent

from WSPs was found to contain maximum of 143 tons/yr of nitrogen and 14 tons/yr of phosphorus from Manzese.

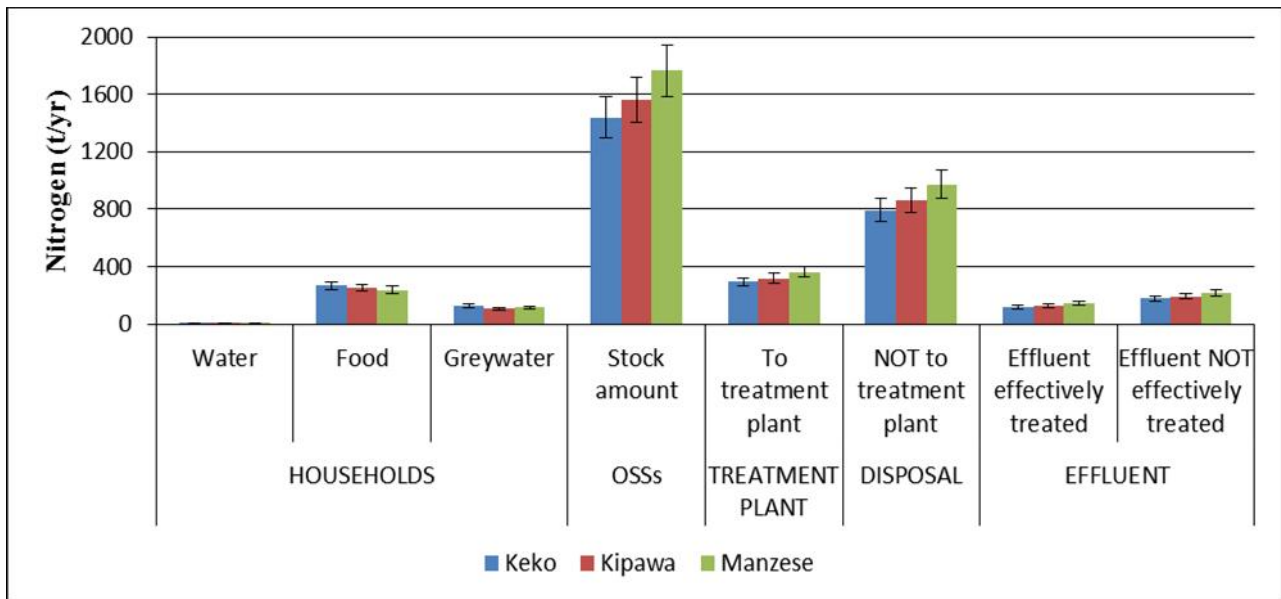
The amount of nitrogen disposed of from Keko area was estimated to be 0.008 tons/ca/yr, which is least amount in this study, found to be highest when compared to per capita amount in other studies. Meinzinger *et al.* (2009) in the town of Arba Minch in Ethiopia (70,000 inhabitants) found that nitrogen content of 0.0038 tons/ca/yr was disposed to the soil. In accordance with Yiougo *et al.* (2011), about 0.0039 tons/ca/yr of nitrogen is discharged in the soil from Pouytenga town in Burkina Faso (72,000 population), which poses groundwater pollution risks.

Table 3: Summary of input data from mathematical formulation to mass balances by STAN software

	Study area				
Parameter	Keko	Kipawa	Manzese	Description/Assumptions	Reference
Population	79,453	74,180	70,507	Population distribution per area	NBS (2017)
Households Process Inflows					
Total Water consumption (L/cap/d)	47.87±1.96	43.09 ± 2.42	48.58 ± 2.91	Average from household questionnaire survey	This study
Water for bathing (L/cap/d)	27.24±0.27	19.99±0.19	21.66±0.22	Average from household questionnaire survey	This study
Food (kg/d)	8258.34 ±825.83	7710.27 ± 771.03	7328.49 ± 732.85	Provided by FAO; uncertainty of 10%	FAO (2013)
Energy-charcoal (tons/d)	508.5 ± 50.85	474.75±47.48	451.24±45.12	Charcoal consumption	Msuya et al. (2011); Meinzinger (2010).
Process Outflow					
Excreta-wet weight (g/cap/d)	520 ±173.2			Faeces generation	Chaggu (2004); Afolabi and Sohail (2017)
	1500 ±722.5			Urine generation	
Containment inflow (kg/cap/d)	25.96 ± 0.92	19.81 ± 0.59	21.22 ± 0.69	Average amount of water for bathing in each area	This study
Greywater (kg/cap/d)	9.94 ± 0.55	12.51 ± 1.22	15.215 ± 1.49	75% of water consumption minus water from bathroom	This study
Onsite sanitation system Process Inflows					
Excreta (g/cap/d)	1500 ± 895.7			Faeces and urine generated	This study
Greywater (kg/cap/d)	8.15 ± 0.45	9.88 ± 0.96	7.15 ± 0.70	82.0% (Keko), 79.34% (Kipawa) and 46.74% (Manzese) of water from bathroom	This study
Process Outflow					
Faecal sludge to treatment plants (kg/cap/yr)	1.12 ± 0.16	1.19 ± 0.19	1.77 ± 0.33	27% of FS Emptied (13.93% of FS generated)	This study
Faecal sludge NOT to treatment plants (kg/yr)	3.03 ± 0.42	3.24 ± 0.53	4.79 ± 0.88	73% of FS Emptied (37.67% of FS generated)	This study
Gases generated from septic (kg CH ₄ /yr)	141,637.68	105,189.09	37,135.68	Methane emission from septic tanks; uncertainty of 10%	Orner and Mihelcic, (2018); IPCC (2006)
Gases generated from pit latrine (kg CH ₄ /yr)	189,279.45	265,076.52	343,933.57	Methane emission from pit latrines: uncertainty of 10%	

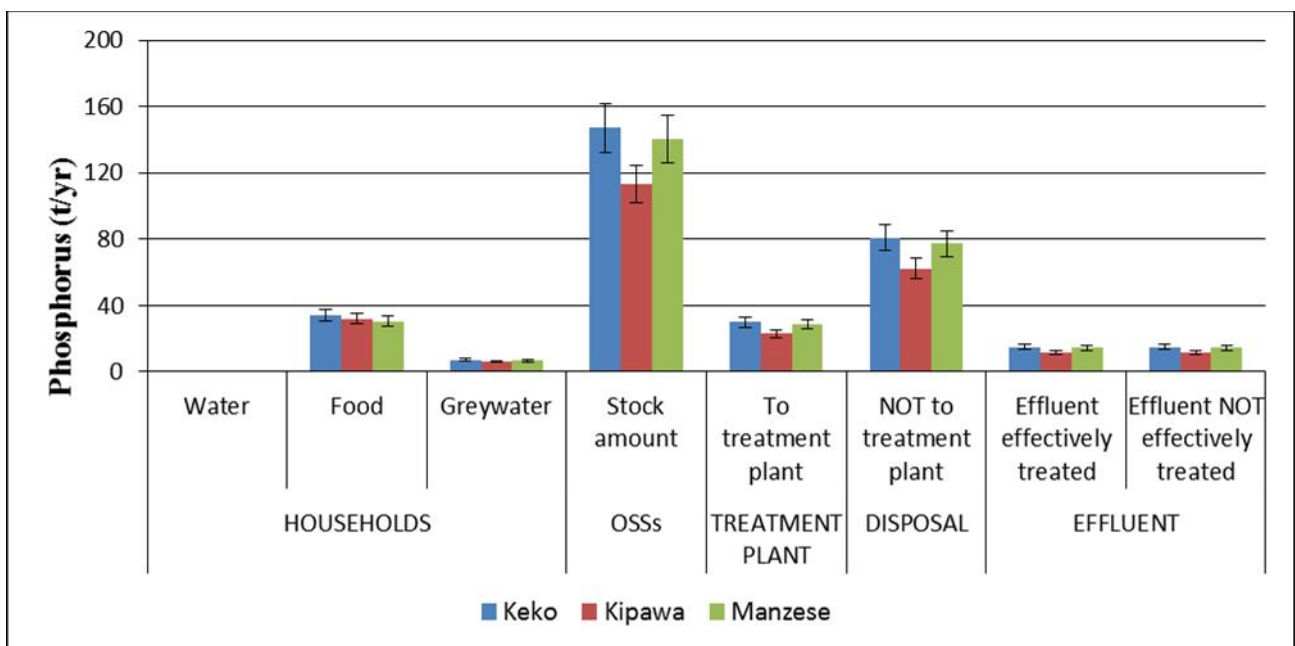
Material Flow Analysis as a Decision Supporting tool for Faecal Sludge Resource Recovery: Mathematical formulation and quantification

Faecal sludge treatment plant Process Inflows					
FS to treatment plants (kg/yr)	1.12 ± 0.16	1.19 ± 0.19	1.77 ± 0.33	27% of FS Emptied (13.93% of FS generated)	This study
Process Outflow					
Effectively treated FS (kg/yr)	0.56 ± 0.08	0.59 ± 0.095	0.89 ± 0.17	50% of FS enters the treatment plants	This study
Not effectively treated FS (kg/yr)	0.56 ± 0.08	0.59 ± 0.095	0.89 ± 0.17	50% of FS enters the treatment plants	This study
Gases from treatment plants (kg/yr)	9.723±0.97		Methane emission		Orner and Mihelcic (2018); IPCC (2006)
Nutrients concentrations in materials					
N in potable water (mg/L)	1.21± 0.10		Concentration in individual amount of water consumed		Meinzinger (2010)
N in food (kg/yr)	$C_{N_{food}} = \frac{a_{TFP}}{6.25}$		Expressed by per capita food consumption a_{food} and conc. of nitrogen in food as protein a_{TFP}		Meinzinger (2010); FAO (2013)
N in greywater (mg/L)	121±69.85		Average amount calculated		Jonsson <i>et al.</i> (2004)
N in excreta (g/cap/d)	7.514±0.751		N= 0.13* Total food protein; 10% uncertainty		Calculated based on FAO (2013); Jonsson <i>et al.</i> (2004)
P in potable water (mg/L)	0.11 ± 0.01		Adopted amount with 10% uncertainty		Meinzinger (2010)
P in food (g/cap/yr)	432 ± 43		Adopted amount with 10% uncertainty		Meinzinger (2010)
P in greywater (mg/L)	7± 4.04		Average amount calculated		Jonsson <i>et al.</i> (2004)
P in excreta (g/cap/d)	1.16±0.11		P = 0.011* (Total food protein + vegetal food protein); 10% uncertainty		Calculated based on FAO (2013); Jonsson <i>et al.</i> (2004)



OSSs = Onsite Sanitation Systems

Figure 7: Amount of Nitrogen flow with materials along sanitation service chain processes (t/yr)



OSSs = Onsite Sanitation Systems

Figure 8: Amount of Phosphorus flow with materials along sanitation service chain processes (tons/yr)

Different systems are available that allow the recovery of nutrients from wastewater flows that suit the specific conditions. These include the introduction of composting or urine diversion systems to allow the use of collected materials for agriculture. In accordance with

Meininger (2010), application of these systems may recover about 17% of nitrogen and 25% of phosphorus generated in Arba Minch City of Ethiopia.

Limitation of Results

Material flow analysis method was used to quantify both materials and nutrients flowing to the specified system. By focusing on material analysis at a community level, the use of MFA in this study encountered some limitations include;

- The lack of data for validation of output of input data when using STAN software at this stage of the study.
- The MFA does not consider social-cultural and health consideration aspects to a community as consumers of products to be produced. These factors might limit the implementation of faecal sludge recovery and reuse for agriculture and energy.
- MFA method is static because it uses one-year temporal boundary for evaluation. To cover several years for comparison, large data set is required.

CONCLUSIONS

From the results of this work it can be concluded that water was the main material imported to the system whereby a person consumes on average 17.0 tons/cap/yr of water, which generates 6.6 tons/cap/yr of greywater disposed to water bodies and an open environment without treatment. Onsite sanitation systems were the major pollutants of the environment and water bodies contributing more than 2 tons/cap/yr of faecal sludge, which was disposed of through seepage of unlined systems to the soil or illegally disposed of in the environment. About 0.48 tons/cap/yr of faecal sludge is disposed of from treatment plants without effective treatment.

Along sanitation service chain, nutrients are not captured for utilization. From treatment plants, a small quantity of nutrients remained are further disposed of with effluents to water bodies, which in accumulation may impact the environment and ecology of the water bodies.

Lack of proper faecal sludge and wastewater management in unplanned settlements encourages people to practice illegal faecal

sludge disposal to the environment. This was evident from the large amount of nutrients discharged to the environment without treatment, which was 37.7% of the faecal sludge that emptied from onsite sanitation systems. To remove nutrients from the water stream, municipalities and responsible authorities need to put resource recovery in sanitation plans from the initial stage. Capacity building, incentives and education on resource recovery to communities are need, important for the proposed projects to sustain.

Acknowledgement

Sincere thanks are extended to the Swedish International Development Cooperation Agency (SIDA) for funding the SUSTAIN project in the Department of Water Resources at University of Dar es Salaam, Tanzania. Special thanks to Lund University Centre for Sustainability Studies (LUCSUS) at Lund University, Sweden for co-supervising the project and their material support.

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